

Thermal Simulations of a Proton CT Calorimeter Detector

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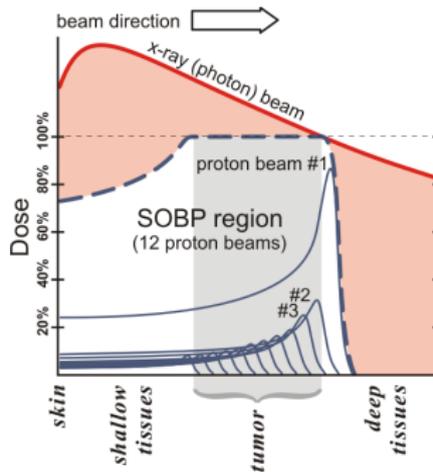
on behalf of Bergen proton CT collaboration
([full collaboration list](#))

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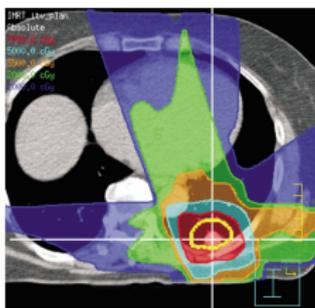
Forum on Tracking Detector Mechanics 2021, 19 May 2021

Motivation: improve proton therapy

- Original idea by Wilson in 1946
- Widespread in the last 20 years
- More advantageous dose distribution due to Bragg-peak
⇒ less side effect



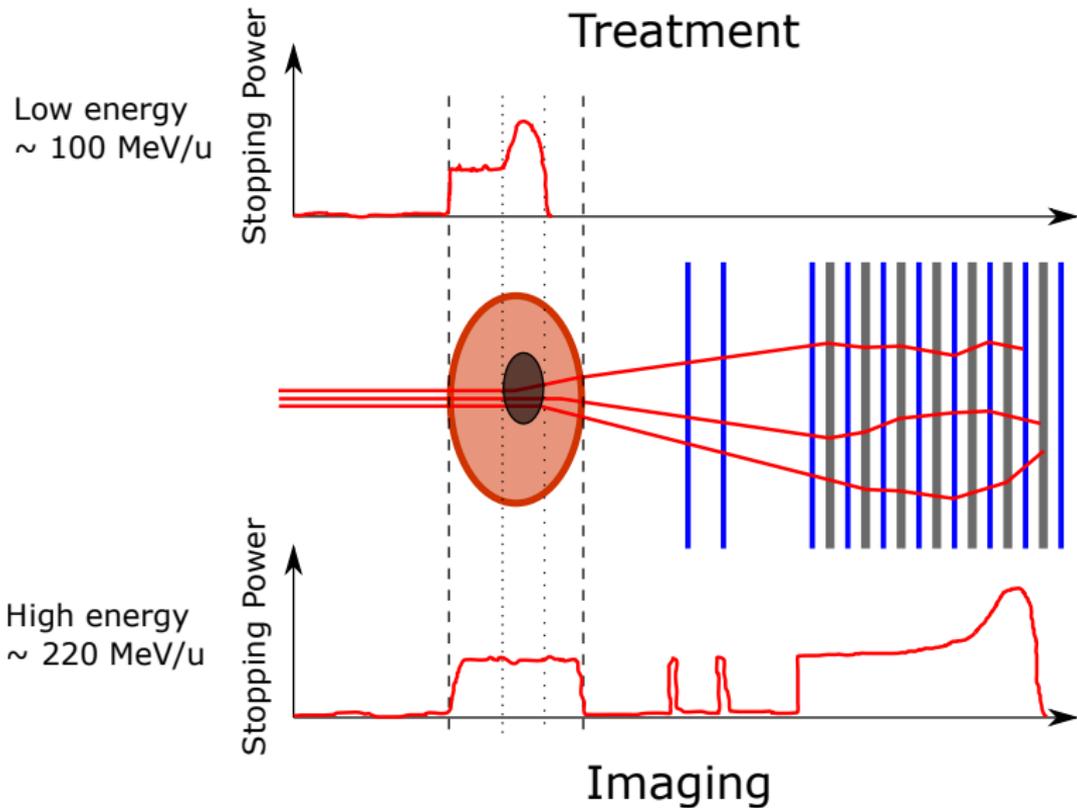
X-ray



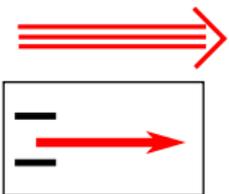
Proton



Proton therapy and proton imaging



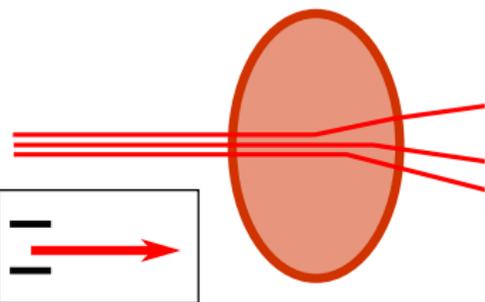
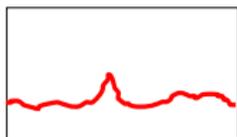
Introduction: how Bergen pCT calorimeter works?



Incoming vector
and energy

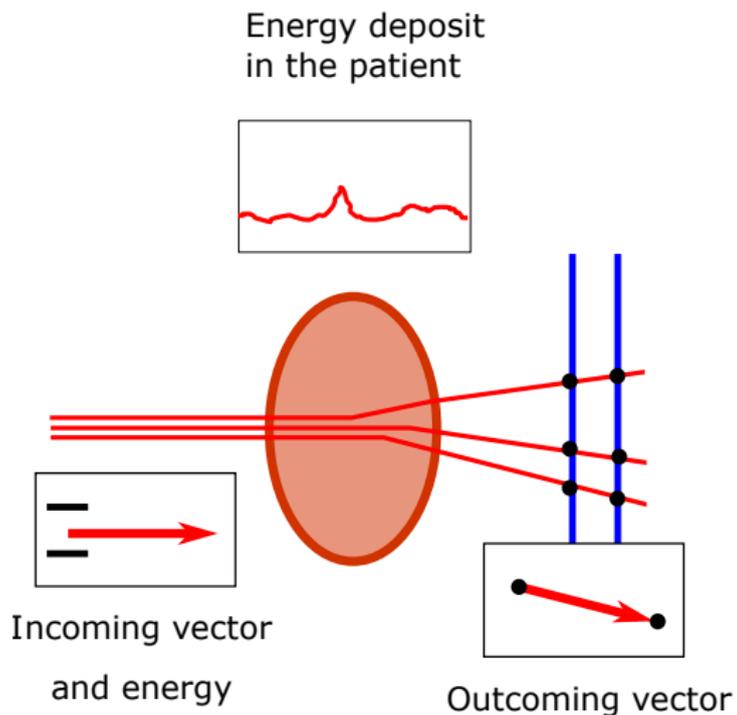
Introduction: how Bergen pCT calorimeter works?

Energy deposit
in the patient

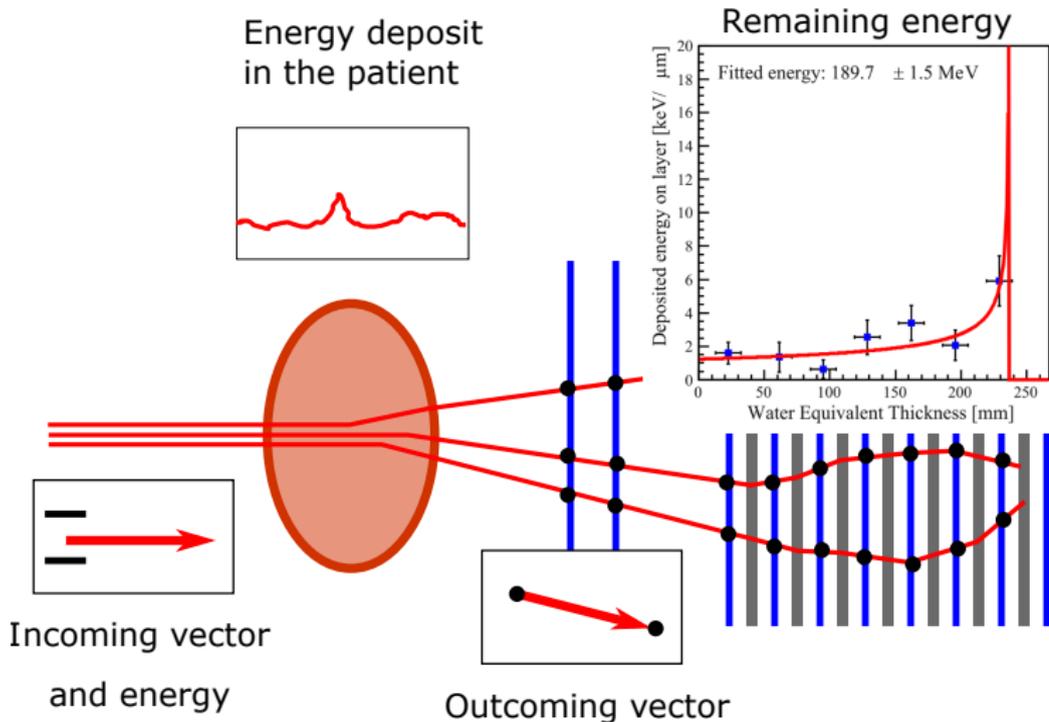


Incoming vector
and energy

Introduction: how Bergen pCT calorimeter works?

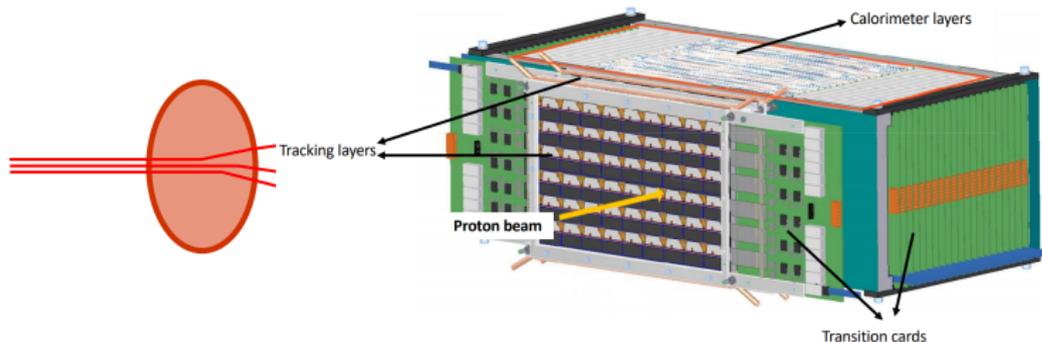


Introduction: how Bergen pCT calorimeter works?



How much heat is generated in the sensitive area?

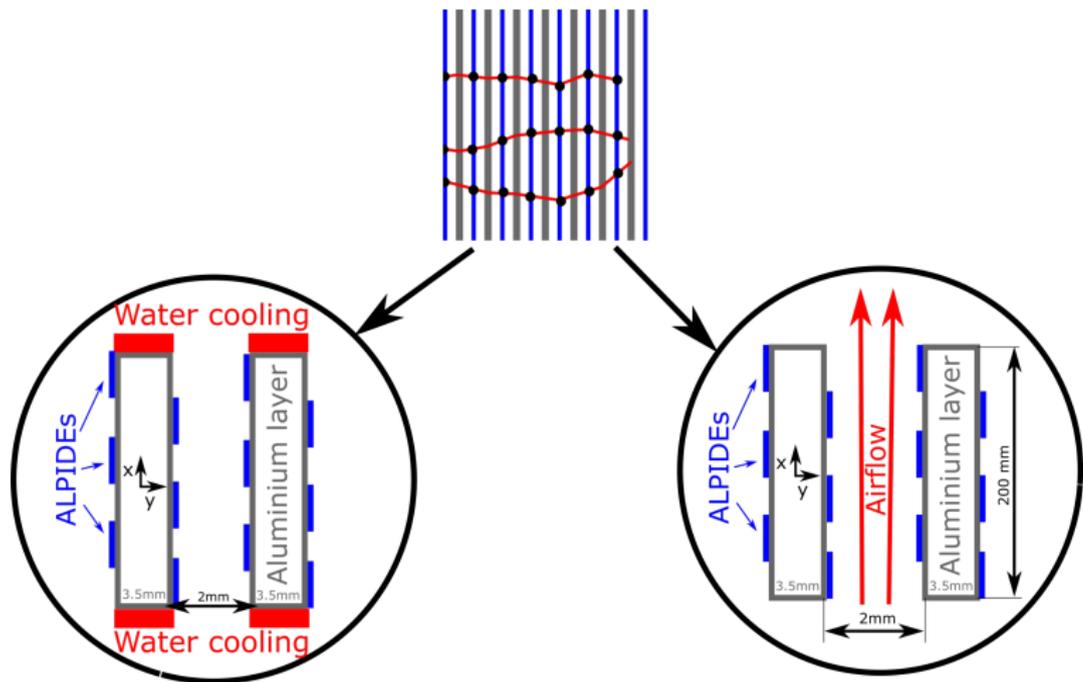
- $4644 \text{ ALPIDEs} \times 300 \frac{\text{mW}}{\text{ALPIDE}} \approx 1.4 \text{ kW}$ heat generation
- $\sim 300 \times 300 \times 200 \text{ mm}^3$ sensitive volume
- Allowed temperature: $T_{\text{Max}} = 30^\circ\text{C}$
- Allowed inhomogeneity in calorimeter part: $\Delta T = 5^\circ\text{C}$



How to transfer heat away? \Rightarrow Two cooling concepts

Water cooling

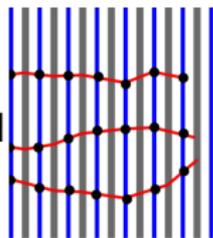
Air cooling



How to transfer heat away? \Rightarrow Two cooling concepts

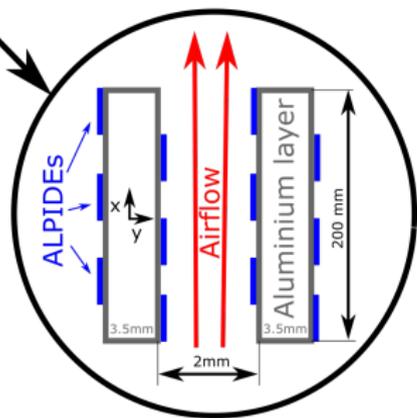
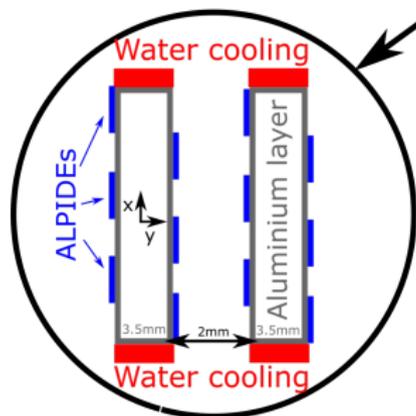
Water cooling

- Intensive water cooling
 \Rightarrow temperature at edge remains constant
 \Rightarrow All heat is transferred away through edge



Air cooling

- Third type of boundary condition in surfaces, which contact with the air flow
- No heat transfer in the other surfaces of the detector



Calculations of water cooling

1D steady state Fourier equation:

$$0 = \lambda \frac{\partial^2 T(x)}{\partial x^2} + q_v ,$$

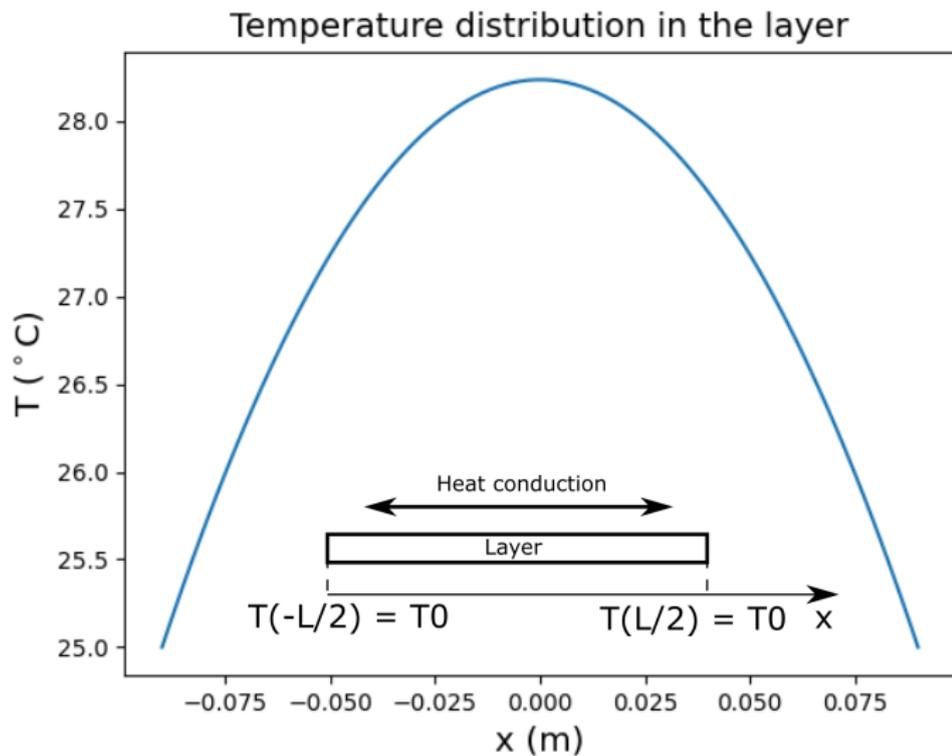
where $T(x)$: temperature , x : coordinate, L : length,
 q_v : volumetric heat generation and λ : thermal conductivity
Boundary conditions, temperatures are T_0 :

$$T(0) = T_0 \quad \text{and} \quad T(L) = T_0 .$$

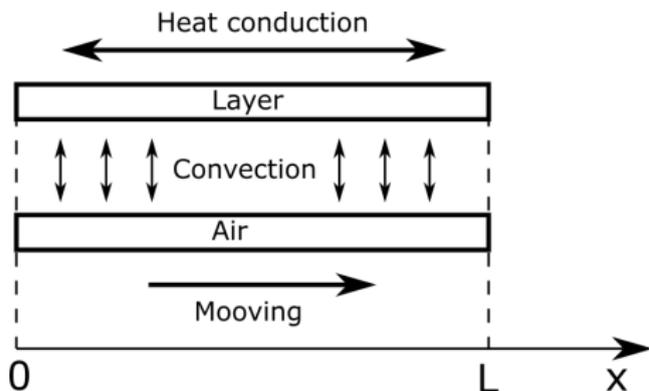
Integrable differential equation \Rightarrow Solution:

$$T(x) = -\frac{q_v}{2\lambda} x^2 + \frac{q_v}{2\lambda} \left(\frac{L}{2}\right)^2 + T_0 .$$

Temperature distribution of water cooling



Calculations of air cooling



The heat conduction in layer:

$$0 = \lambda \frac{\partial^2 T_c(x)}{\partial x^2} - \frac{Q_c(x)}{V_c} + q_0 .$$

The temperature change of airflow:

$$\rho c v \frac{\partial T_a(x)}{\partial x} = \frac{Q_c(x)}{V_a} .$$

The convection between them:

$$Q_c(x) = \alpha A [T_c(x) - T_a(x)] .$$

T_c : layer temp. , T_a : air temp. , Q_c : heat transfer from layer to air, q_0 : volumetric heat generation, V_c : layer volume, V_a : air volume, A : contact area, λ : layer thermal conductivity, ρ : air density, c : specific heat capacity of air, v : airspeed, α : heat transfer coefficient between layer and air.

Calculations of air cooling

Layer temperature: $T_c(x) = C_1 e^{r_1 x} + C_2 e^{r_2 x} + C_3 x + C_4$.

Air temperature: $T_a(x) = \frac{\lambda}{\rho c v} \frac{\partial T_c}{\partial x} + \frac{1}{\rho c v} q_0 x + \frac{1}{\rho c v} \hat{c}$.

$C_1, C_2, r_1, r_2, C_3, C_4$ and \hat{c} are constants based on: $\alpha, A, L, \rho, c, v, \lambda, V_c$ and V_a .

Boundary conditions:

$$\left. \begin{aligned} T_a(x)|_{x=0} &= T_0 && \Rightarrow \hat{c} \\ \frac{\partial T_c(x)}{\partial x} \Big|_{x=0} &= 0 \\ \frac{\partial T_c(x)}{\partial x} \Big|_{x=L} &= 0 \end{aligned} \right\} \Rightarrow C_1 \text{ and } C_2$$

Heat transfer coefficient (α) based on Tachibana and Fukui^[1]:

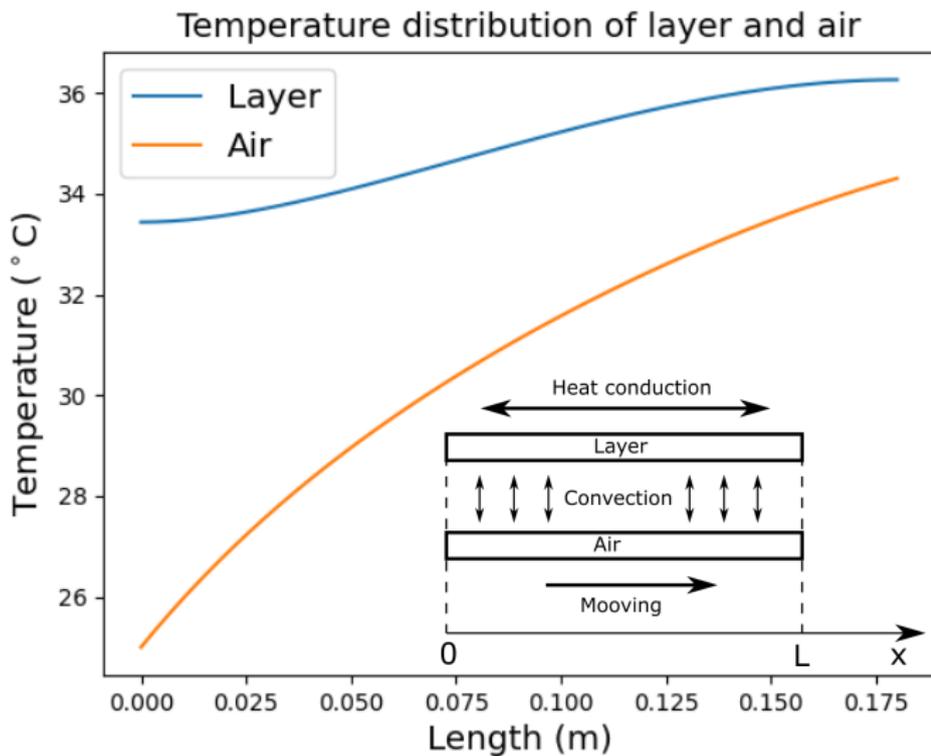
$$\alpha \approx \frac{\lambda}{D_e} 0.017 \left(1 + 2.3 \frac{D_e}{L}\right) \left(1 - \frac{\pi D_e}{K}\right)^{0.45} \text{Re}^{0.8} \text{Pr}^{0.33},$$

where λ : thermal conductivity, K : width of the gap, L : length of the gap, d : thick of the gap, $D_e = 4 \frac{K \times d}{2K + 2d} \approx 2d$: equivalent diameter, Re : Reynolds number, Pr : Prandtl number.

Warning! Strong extrapolation: α was measured for turbulent flows and we use them for laminar \rightarrow upper estimates α

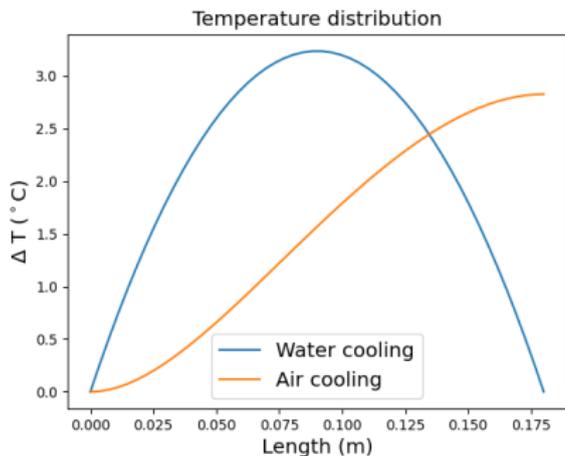
[1]: Fujio Tachibana and Sukeo Fukui, Convective Heat Transfer of the Rotational and Axial Flow between Two Concentric Cylinders, Bulletin of JSME, 7(26):385-391, 1964.

Temperature distribution of air cooling



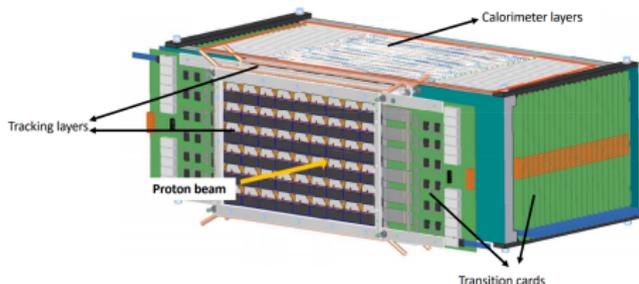
Comparison of the two cooling strategy

- **Water cooling:** $T_{\max} = 23.2 \text{ }^{\circ}\text{C}$ and $\Delta T = 3.2 \text{ }^{\circ}\text{C}$
- **Air cooling:** $w = 10 \frac{\text{m}}{\text{s}}$ and $\alpha = 73 \frac{\text{W}}{\text{m}^2 \times \text{K}} \rightarrow$
 $T_{\max} = 36.3 \text{ }^{\circ}\text{C}$ and $\Delta T = 2.8 \text{ }^{\circ}\text{C}$
- Requirement 1: $T_{\max} < 30 \text{ }^{\circ}\text{C}$, only water cooling meets
- Requirement 2: $\Delta T < 5 \text{ }^{\circ}\text{C}$, both concept meet



Summary

- Bergen pCT Collaboration is developing a proton CT
- Data taking time: main limitation of available prototypes
⇒ Goal: overcome this limitation
- First test results expected within two years
- We investigated two cooling system concepts
- Water cooling met all requirements ⇒ under construction now



Thank you for your attention!

Members of the Bergen pCT collaboration: University of Bergen, Norway; Helse Bergen, Norway; Western Norway University of Applied Science, Bergen, Norway; Wigner Research Center for Physics, Budapest, Hungary; DKFZ Heidelberg, Germany; Heidelberg Ion-Beam Therapy Center (HIT), Germany; Utrecht University, The Netherlands; RPE LTU, Kharkiv, Ukraine; Suranaree University of Technology, Nakhon Ratchasima, Thailand; China Three Gorges University, Yichang, China; University of Applied Sciences Worms, Germany; University of Oslo, Norway; Eötvös Loránd University, Budapest, Hungary

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